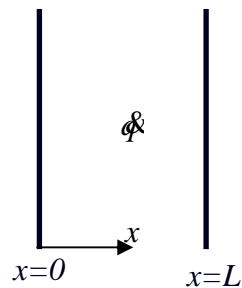


## Module 2: Short questions

1. How does transient heat transfer differ from steady state heat transfer?
2. What is meant by the term “one-dimensional” in the context of conduction heat transfer?
3. What is meant by thermal resistance? Under what assumptions can the concept of thermal resistance be applied in a straightforward manner?
4. For heat transfer through a single cylindrical shell with convection on the outside, there is a value for the shell radius for a nonzero shell thickness at which the heat flux is maximized. This value is
  - (A)  $k/h$
  - (B)  $h/k$
  - (C)  $h/r$
  - (D)  $r/h$
5. The steady temperature profile in a one-dimensional heat transfer across a plane slab of thickness  $L$  and with uniform heat generation,  $\dot{\phi}$ , has one maximum. If the slab is cooled by convection at  $x = 0$  and insulated at  $x = L$ , the maximum occurs at a value of  $x$  given by



- (A) 0
  - (B)  $\frac{L}{2}$
  - (C)  $\frac{\dot{\phi}}{k}$
  - (D)  $L$
6. Consider a cold canned (typically cylindrical in shape) drink left on a table. Would the heat transfer be steady or transient? Would you model the heat transfer as one-, two-, or three-dimensional? Also, which coordinate system would you use to analyse this heat transfer problem?