

# BIOMETHANATION

Insoluble Organics

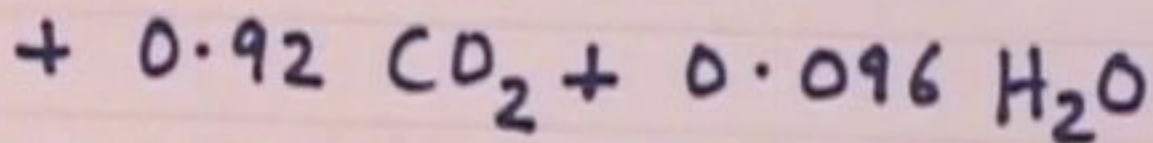
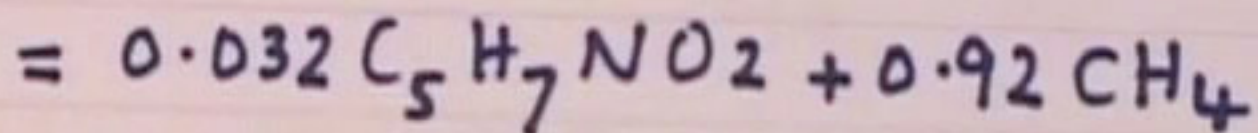
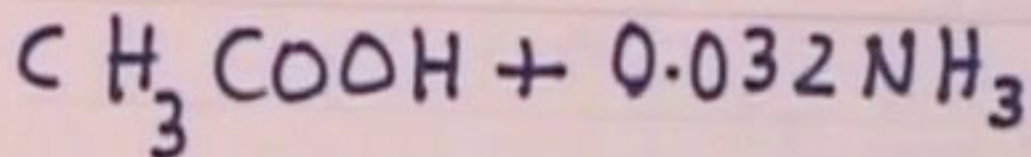


Extra Cellular Enzymes  
Solubilizes organics

volatile ↓ Acids by acid  
producing bacteria (Acetic Acid)  
CO<sub>2</sub>, H<sub>2</sub>)

Gasification ↓ by Methane producing  
bacteria (CH<sub>4</sub>, CO<sub>2</sub>)

# STOICHIOMETRY



$$\mu = \mu_m \left[ \frac{1}{1 + \frac{K_s}{Hs} + \frac{Hs}{K_1}} \right]$$

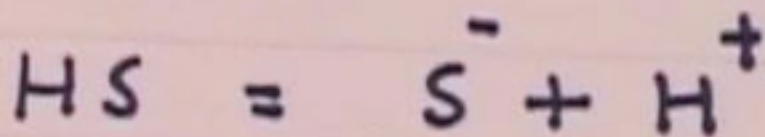
Graef & Andrews  
(1974)

$$\underline{\underline{Hs = H^+ + S^-}}$$

$$\mu = \mu_m \left[ \frac{1}{1 + \frac{K_s}{HS} + \frac{HS}{K_i}} \right]$$

$$K_s = 0.0333 \text{ mmol/L}$$

$$K_i = 0.667 \text{ mmol/L}$$



$$K_a = \frac{S^- H^+}{HS}$$

$$pK_a = 4.5 \quad pH = 6.8$$



$$(H_s)_{opt} = \sqrt{K_s K_i}$$

$$\sqrt{(0.0333)(0.667)}$$

$$= 0.15 \text{ mmol/L}$$

$$D = \mu = 0.4 \left[ \frac{1}{1 + \frac{0.0333}{0.15} + \frac{0.15}{0.667}} \right]$$

$$= 0.27/d.$$



$$D = \mu = 0.27/d$$

$$V: F/D = \frac{3000 \text{ M}^3/d}{0.27/d}$$

$$= 11111 \text{ M}^3$$

$$HS = S^- H^+ / K_a$$

$$S^- = \frac{0.15 \cdot 10^{-4.5}}{10^{-6.8}} = 29.9 \frac{\text{mmol}}{\text{L}}$$

$$= 1795 \frac{\text{mg}}{\text{L}}$$

$$S = \bar{S} + HS$$

$$1795 + 9 = \overset{1804}{\cancel{2004}} \text{ mg/L}$$

$$\text{COD LOSS} = F(S_0 - S) \text{ kg/d}$$

$$\overset{6-1.8}{\cancel{6-0}} 3000 (\cancel{6-0}) =$$

$$12600 \text{ } \cancel{12000} \text{ kg/d}$$

$$Y_{\text{CH}_4/S} = (0.92) \frac{16}{60} = 0.24$$

$$Y_{\text{CO}_2/S} = (0.92) \frac{44}{60} = 0.67$$



Methane Production

$$= (12600) 0.24$$

$$= \frac{3025}{2880} \text{ kg/d}$$

CO<sub>2</sub> Production

$$(12600)(0.67) = \frac{8000 \text{ kg}}{8440 \text{ d}}$$



Methane Fraction in gas

$$= \frac{2880}{2880 + 8000} = 0.26.$$

So  $\text{CH}_4$  is 26% in biogas

GAS THERMAL VALUE =

$$(0.26)(14000) = 3640 \frac{\text{kcal}}{\text{kg}}$$

$$= 4918 \text{ kcal/m}^3$$

[NOTE 1 kg Gas = 0.74 m<sup>3</sup>]



Effluent ~~is~~ <sup>1804</sup> 2000 mg/L

Effluent Treatment

$$D = \frac{1}{B} \frac{\mu_{m} S}{K_s + S}$$

$$D = \frac{1}{0.3} \frac{0.3 \times 10}{10 + 10} = 0.5/d$$

$$V = F/D = \frac{6000}{0.5} \frac{3000}{0.5}$$

6000 M<sup>3</sup>

E TP  
 COD LOSS  $(3000) \frac{2}{1.80} = \frac{6000}{1.80} = 3333 \text{ kg/d}$   
~~12000 kg/d~~  
 5400 kg/d

Oxygen Supply Needed

@  $1 \text{ Kg O}_2 / \text{KWH} = \frac{5400}{12000} \text{ KWH/d}$

POWER PRODUCTION =

$(\cancel{2580}) \frac{140000 \times 0.3 \text{ (OR } 0.2)}{860}$

$\cdot 14770$   ~~$\cdot 14065$~~   $\text{KWH/d}$

$\cdot 9847$   ~~$\cdot 9375$~~   $\text{KWH/d}$

KWH/d

860 Kwh  
 = 1 KWH





Alcohol : 40 TON/D

$$F (S_0 - S) 0.4 = 40000/24$$

$$F = \frac{40000}{24(90)(0.4)} = \frac{1111 \dot{M}^3}{24 D}$$

$$= 46 M^3/D \cdot HR$$

$$P = (S_0 - S) \gamma_P / \gamma_s = (100 - 10) 0.4$$

$$= 36 \text{ kg}/M^3$$

$$\mu = \frac{\mu_m S \exp(-kP)}{K_s + S}$$

$$D = \mu = \frac{(0.5)10 \exp(-0.017 \times 36)}{(2.2 + 10)}$$

$$= \frac{(0.5)(10)(0.542)}{12.2}$$

$$0.22 / \text{HR}$$

$$F = 46 \text{ M}^3 / \text{DHR}$$

$$D = 0.22 / \text{hr}$$

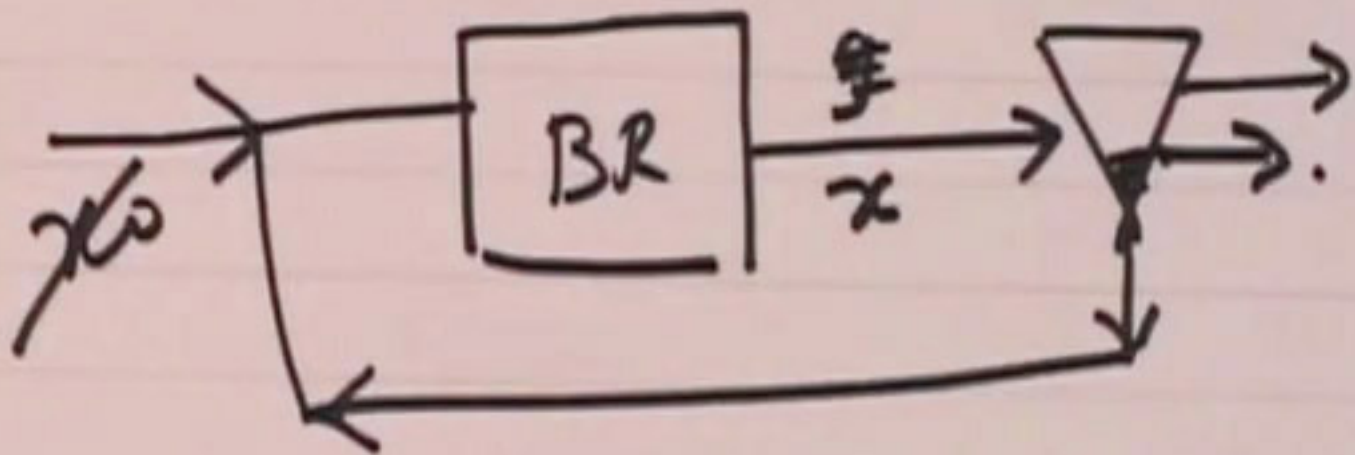
$$V = \frac{46}{0.22} = 206 \text{ M}^3$$

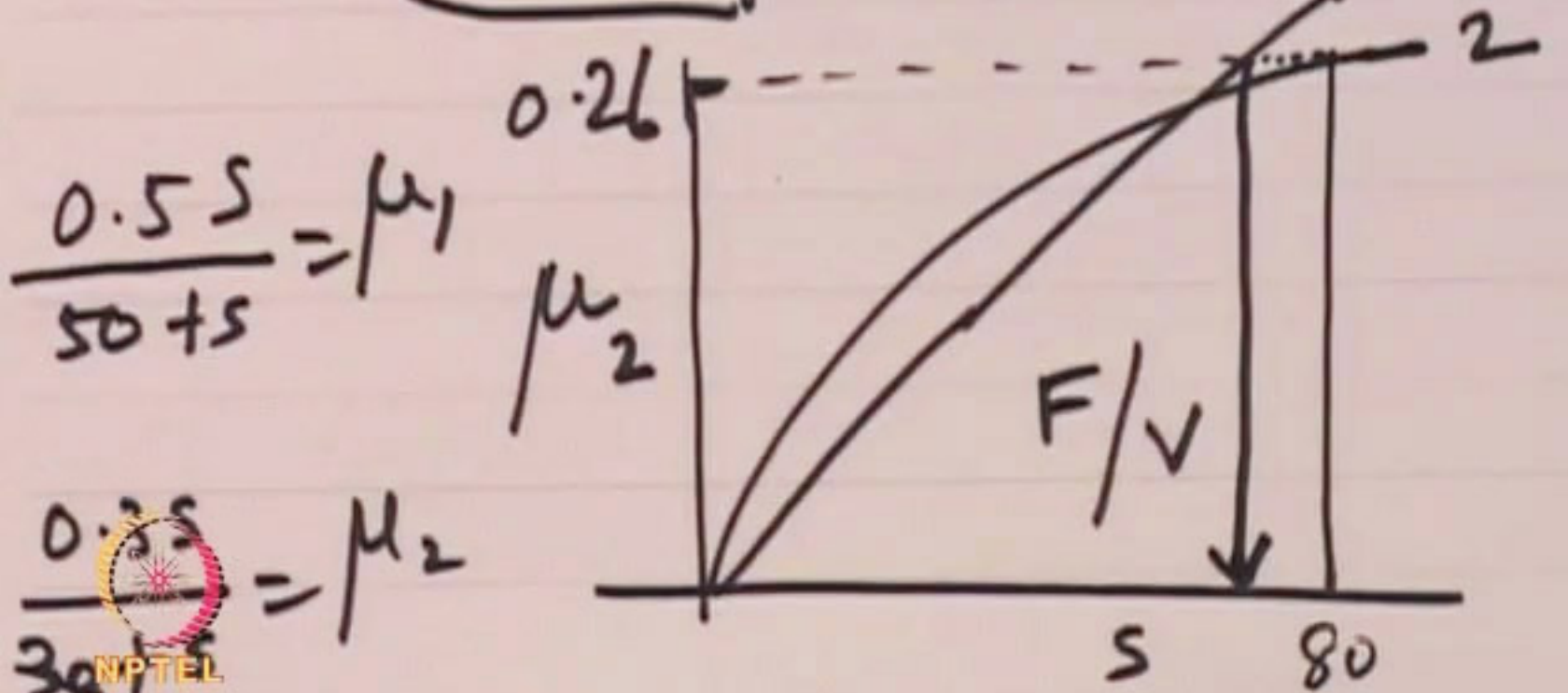
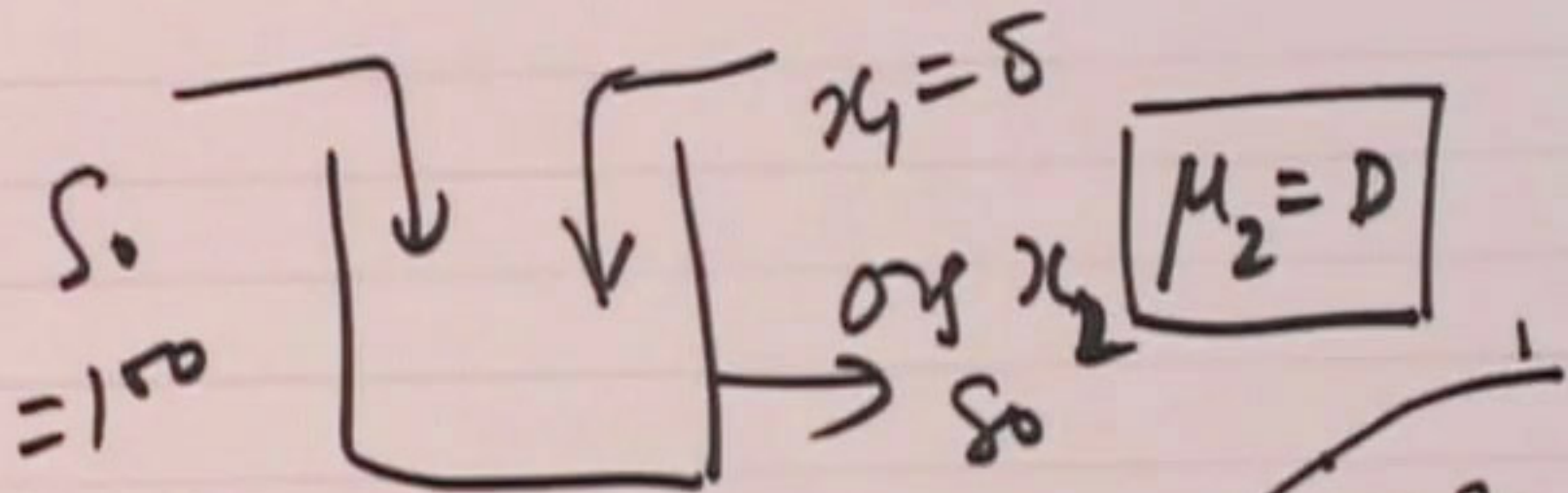
$$\begin{aligned} \text{Productivity} &= DP \\ &= (0.22)(36) \\ &= 7.9 \text{ kg} / \text{M}^3 \cdot \text{hr} \end{aligned}$$

# Fermentation Alcohol Reactor Alternatives

1. Batch
2. Chemostat
3. Immobilized cell Reactor
4. Vacuum Fermentation







$$\frac{0.5S}{50+S} = \mu_1$$

$$\frac{0.3S}{100+S} = \mu_2$$

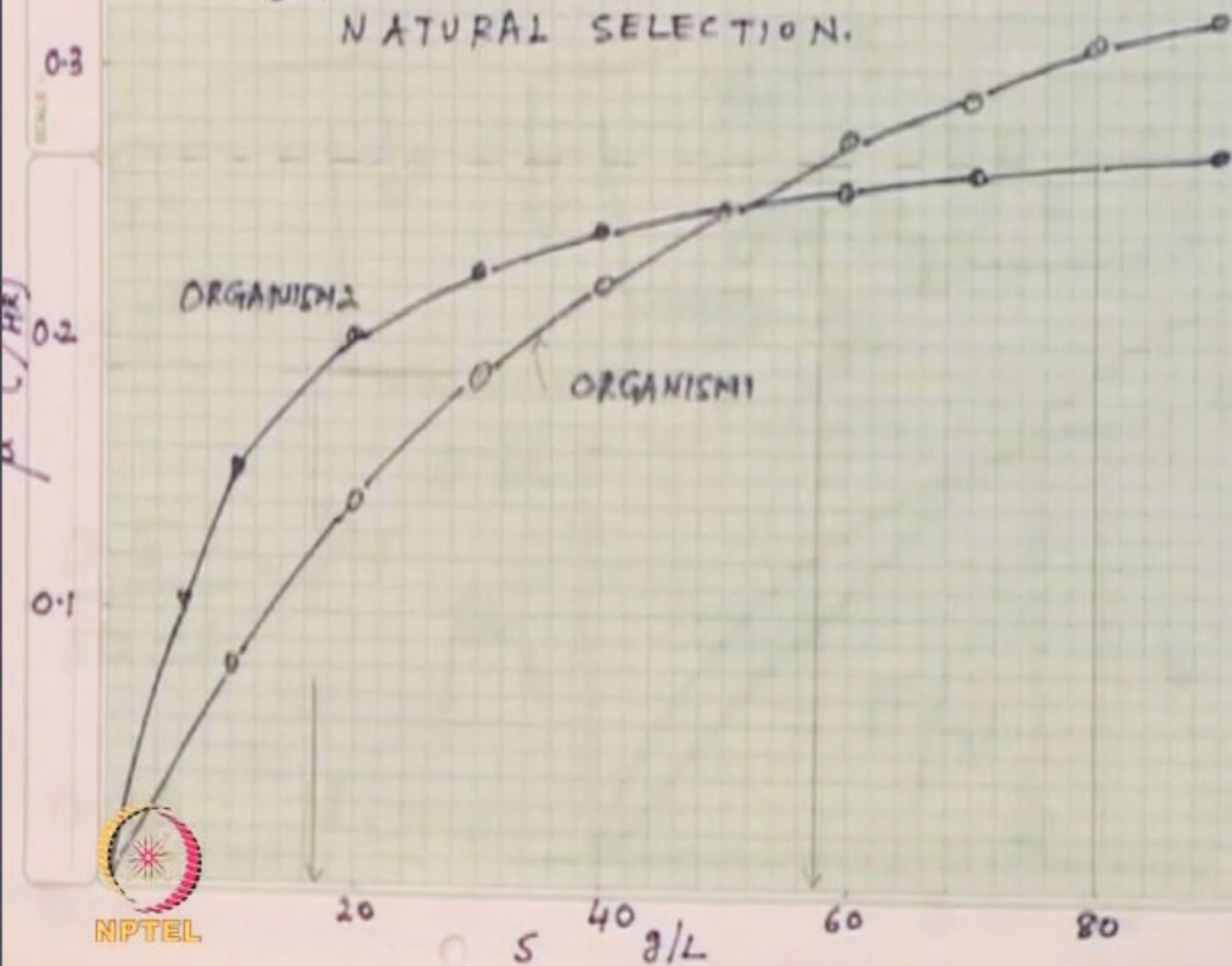


$$\mu_1 = \frac{0.55}{50+S}$$

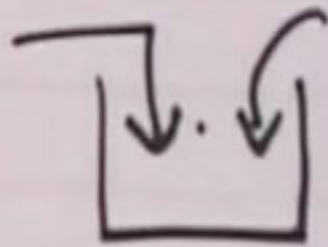
$$\mu_{max} = \frac{\mu_m S}{K_s + S}$$

$$\mu_2 = \frac{0.35}{10+S}$$

NATURAL SELECTION.



$$F x_{10} - F x_1$$



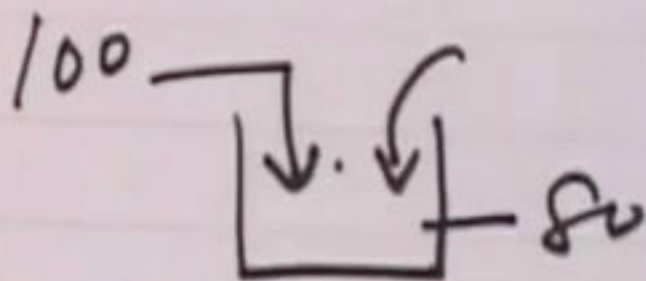
$$F x_{20} - F x_2 + (\mu_2 x_2) v = \frac{d \cdot v x_2}{dt}$$

$$F x_{10} - F x_1 + (\mu_1 x_1) v = \frac{d \cdot v x_1}{dt}$$

$$F S_0 - F S = \frac{(\mu_1 x_1 + \mu_2 x_2) v}{\gamma} = \frac{d V S}{dt}$$

Q2.1

$$F x_{10} - F x_1$$



$$F x_{20} - F x_2 + (\mu_2 x_2) v = \frac{d \cdot V x_2}{dt}$$

$$F x_{10} - F x_1 + (\mu_1 x_1) v = \frac{d \cdot V x_1}{dt}$$

$$F S_0 - F S = (\mu_1 x_1 + \mu_2 x_2) v = \frac{d V S}{dt}$$



$$S_0 = 80; \quad x_2 = 10 \text{ g/L}$$

$$x_1 = 5 (0.001 \text{ g})$$

Q2.2

$$S_0 = 100$$

$$S = 30$$

$$t=0 \quad x_1 = 358/L$$

$$x_2 = 0.0018/L \quad (\text{in } \mu\text{L})$$



Q2.1

$$F x_{10} - F x_1 \quad 100 \quad \downarrow \quad \downarrow \quad 80$$

$$+ \quad \cancel{F x_{20}} - F x_2 + (\mu_2 x_2) \stackrel{V}{=} \frac{d \cdot V x_2}{dt}$$

$$\frac{t=0+}{F} \quad \cancel{F x_{10}} - F x_1 + (\mu_1 x_1) \stackrel{V}{=} \frac{d \cdot V x_1}{dt}$$

$$S_0 = 100 \quad S_0 - F S \stackrel{V}{=} (\mu_1 x_1 + \mu_2 x_2) \stackrel{V}{=} \frac{dV}{dt}$$

$$S_0 = 80 \quad x = 10 \text{ cl}$$